

MICROBIOLOGICAL PRODUCTION OF POLYHYDROXBUTYRATES FROM RENEWABLE SOURCES

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ABSTRACT

Plastics play an important role in our daily lives and are used for various purposes. The industry of environmentally friendly products is actively developing in our time, including bioplastics, and much attention of scientists is attracted by biodegradable polymers such as polyhydroxyalacanoates or its subspecies polyhydroxybutyrates, which are synthesized by various microorganisms as a reserve substance, and are also the most acceptable replacement for conventional synthetic plastics. However, the cost of large-scale production of such a biodegradable polymer is not competitive with its wide distribution. Studies of the microbial production of polyhydroxybutyrates should be aimed at identifying cost-effective substrates, as well as determining the appropriate strain of the body for production. These biopolymers have a number of specific properties, such as biodegradability and compatibility with living body tissue, which opens up great opportunities for their use in practice. The final product of polyhydroxybutyrates biodegradation in the environment is water and carbon dioxide, and in a living organism 3-butobutyric acid. The main focus of this review was the production of bioplastics from various economical substrates using various types of bacteria.

Keywords: biopolymer, polyhydroxybutyrate, polyhydroxyalacanoate, renewable source, microbial production, cheap carbon sources; periodic culture.

INTRODUCTION

Plastic has a special place in the modern world and is used in various fields of activity, such as packaging, construction materials, consumer goods and much more. About 100 million tons of plastics are produced annually in the world [1]. As we know, a synthetic polymer consists of a petrochemical material, which can become a source of environmental pollution for a long time and harm animals. The fight against plastic waste continues, in particular, even in developed countries where there are plastic processing points, not all types of plastic are accepted. And in no other way do plastic polygons accumulate or move, getting blown into the oceans, which exacerbates the situation, posing a threat to wildlife.

The global production of petroleum-based synthetic oils was around 270.0 million tons in 2007. In some developed countries, the process of plastic processing is underway, in this area, countries such as Germany, Japan, South Korea, Slovenia, Austria and others have already achieved some success. About 30% of plastic is

recycled or recycled in EU countries, about 10% in the USA, while in the vast majority of developing and poor countries this does not happen or is carried out on a very small scale. However, plastic recycling is expensive and not always effective. First of all, garbage collected requires preliminary labor-intensive manual sorting. After this, the plastic has to be cleaned and crushed into small particles. At the same time, current technologies do not allow preserving the properties of plastic: during processing, it turns yellow, loses its presentation and is no longer suitable for the production of food packaging, that is, it cannot be fully used again [2].

And yet, we cannot completely abandon the use of plastic, because it is difficult to imagine a medical institution without disposable syringes or other irreplaceable items of use, but replacing them with biocompatible and also biodegradable plastic is more appropriate and environmentally friendly. The industry of environmentally friendly products today is actively developing, including bioplastics, from starch and glucose syrups. Bioplastics are produced in three directions: by synthesis from monomers, by fermentation by microorganisms, and by polymerization of lactic acid derivatives (polylactides). And now, 80% of all waste in the world is made up of plastics that are not degradable for a long time of about 100 years.

Polyhydroxyalcanoates (PHA) are the most acceptable replacement for traditional plastics among biodegradable plastics [3], however, the cost of a biological product by 40% is determined by the price of a carbon source, therefore, the widespread production of PHA is constrained. The most common in a wide range of high molecular weight microbial polyhydroxyalkanoates is poly-3-hydroxybutyrate (PHB). Poly (hydroxybutyric acid) (PHB) and other biodegradable polyesters are promising candidates for the development of environment-friendly, totally biodegradable plastics. These polyesters include repeating hydroxyacyl monomers of the general formula: $[-O-CH(R)-CH_2-CO-]_n$, where $R = CH_3$, they are synthesized and stored in the cell cytoplasm as water-insoluble inclusions by various microorganisms and have important commercial value due to their thermoplastic properties and biodegradability. The physical properties of PHB are similar to those of some common plastics. PHB is an intracellular lipid polymer used by bacteria, in the form of energy in conditions of nitrogen deficiency. At present, more than 300 species of PHB synthesizing bacteria are known, in particular, such as *Ralstonia eutropha* PHA, *Azotobacter beijerinckia*, *Bacillus megaterium*, *Pseudomonas oleovorans*, various nitrogen-fixing microorganisms found in the root nodules of the legume family, and many others [4]. However, the global PHA market is still small compared to the production of petroleum-based polymers. According to the latest market data published by European Bioplastics [5], global biopolymer production reached 2.11 million tons in 2018, including 1.4% PHA.

Although numerous types of bacteria produce PHA and only a few of them are able to accumulate polyesters in large quantities and can be used on a commercial scale fermentation and have advantages that can be divided into 3 aspects: 1) the ability to produce large amounts of intracellular polymer; 2) the ability to grow on a wide range of carbon sources, including found in agricultural waste streams; and 3) penchant for genetic manipulation. for the production of large quantities of polymer [6]. PHA have thermoplasticity, optical activity, antioxidant properties, piezoelectric effect and, most importantly, they are characterized by biodegradability and biocompatibility. The widespread use of PHA makes the product attractive for commerce, PHA have thermoplasticity, optical activity, antioxidant properties, a piezoelectric effect and, most importantly, they are characterized by biodegradability and biocompatibility to produce flexible films, nonwoven materials, medical threads, semi-permeable membranes, various containers, packaging and etc Since PHA is synthesized from various bacteria, this makes it possible to obtain a polymer with

desired properties with special methods of their cultivation. In the general context of nanomedicines, polymer-based drug delivery systems have generated rapidly growing interest and much effort has been put into combating various diseases, including cancer. Polyester nanoparticle drug delivery systems, including polymer-drug conjugates and amphiphilic block copolymers, are the main class with promising results, especially for those derived from poly (3-hydroxybutyrate) (PHB).

It should be noted that the use of PHA in the manufacture of medical materials requires careful control of the polymer composition, they must be biocompatible, which means they cannot cause serious immune reactions when introduced into the soft tissues or into the blood of the host. PHA materials should also not cause immune reactions during degradation in the body. For suture materials must meet the required strength, toughness and resilience. As a rule, PHA polymers decompose under the influence of nonspecific lipase and esterase in nature.

PHB biosynthesis process. Of considerable interest is the evidence that PHA can consist of various hydroxyalkanoate monomers, and the cloning of genes for its biosynthesis. This led to the production of PHA with various physical properties using genetically engineered microorganisms. The abundant synthesis of PHA requires certain conditions that provide some changes in the synthesis and accumulation of PHA in the metabolism in the cell, the state of the redox process in the cytoplasm and the intracellular ratio of acetyl-CoA / CoA [7].

PHA biosynthesis is divided into three main phases according to [8] (Fig. 1). In phase I, a suitable carbon source enters the cell through simple diffusion or specific transport systems located in the cytoplasmic membrane. In phase II, the compound is intracellularly metabolized to hydroxyacyl-CoA, and it will be a substrate of PHA synthase. In phase III, PHA synthase forms oxo ester bonds, releasing CoA [9].

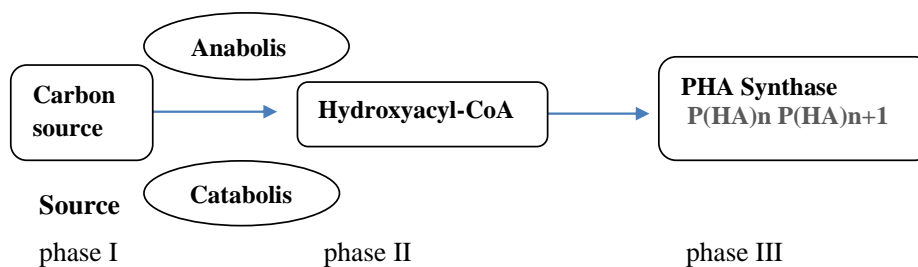


Fig. 1. Phases in the biosynthesis of PHA

Also, environmental conditions for bacterial growth, under unbalanced growth conditions, namely in the absence of one of the macro elements in the medium (nitrogen, phosphorus) or oxygen deficiency, when acetyl-CoA is not included in the tricarboxylic acid (CTK) cycle, and the level of free CoA while low, the activation of enzymes for the synthesis of PHA. The last reaction of the synthesis of PHB is catalyzed by the synthesis of PHB (PHAC), which remains covalently bound to the resulting PHB granule [10]. The unique way in the basis of self-assembly was used by translational fusion of proteins of interest to any end of the PHAC, which ultimately made it possible to obtain PHB granules demonstrating various functions of the protein.

Bacillus megaterium is one of the few bacteria that naturally produces PHB. This was first mentioned by Lemoine in 1926, who described the extracellular substance as polyhydroxybutyrate (PHB) [11]. Other advantages of this organism are its large cell size (up to $1.5 \times 4 \mu\text{m}$) and the presence of overexpression systems with strong promoters [12]. *B. megaterium* is a rod-shaped, gram-positive, mainly aerobic, spore-forming bacterium that occurs in various places a habitat. With a cell length of up to $4 \mu\text{m}$ and a diameter of $1.5 \mu\text{m}$ *B. Megaterium* are one of the most famous

large bacteria. Cells are often found in pairs and chains [13], where they are connected by polysaccharides on cell walls. To carry out the synthesis of PHB in *B. Megaterium* cells, various genes of PHB synthase and phasins are involved, which play an important role in the production of PHB and the formation of granules. Phasin, a protein that separates hydrophobic PHB from the cytoplasm. Thus, phasin can inhibit the fusion of individual granules and contribute to the synthesis of PHB by adjusting the ratio of surface area to volume of PHB granules. PHA may also have a protective function to reduce the passive attachment of cytoplasmic proteins to the surface of PHB. Tian-RenLee scientists and others from Yan-Ming National University reported that the PhaQ gene, which is located before the phasin-encoding PhaP gene, encodes a new class of transcriptional regulator that negatively controls the expression of both PhaQ and PhaP. The PHA binding site was identified using gel mobility shift assays and DNase I imprint analysis. They also provided evidence that PHA can sense the presence of PHB in vivo and that artificial PHB granules can inhibit the formation of the PHA-DNA complex by invitro by direct binding to PhaQ. This suggests that PHA is a repressor that responds to PHB [14].

PHB is synthesized from the central metabolite of acetyl-CoA, which requires sequential transformations catalyzed by three enzymes. The last reaction of the synthesis of PHB is catalyzed by the synthesis of PHB (PhaC), which remains covalently bound to the emerging PHB granule [15]. The unique main way of self-assembly was progressively harnessed by fusion of proteins of interest to any end of the PhaC, which ultimately allowed the production of PHB granules displaying various protein functions.

PHA metabolism regulation. PHA biosynthesis is regulated by the activity of β -ketothiolase and acetoacetyl-CoA reductase, while PHA biodegradation depends on the activity of 3-hydroxybutyrate dehydrogenase.

The control of the activation and inhibition of these enzymes is regulated by various compounds that are important factors responsible for their behavior: acetyl-CoA, free CoA and, to a lesser extent, NADP + or NADPH, ATP, pyruvate and oxacetate. In general, high PHA yields are achieved as a result of an excess of carbon and an energy source, together with a decrease in sulfur, phosphorus, nitrogen, or oxygen [16]. Under conditions of oxygen restriction, the synthesis of PHA allows the cell to regenerate its regenerative power, but if sufficient oxygen is available, CoA increases due to the introduction of acetyl-CoA into the carboxylic acid cycle (TCA - also known as citric acid cycle, Krebs cycle, less commonly, Saint-György-Krebs). On the other hand, if sulfur is limited, it stops protein synthesis due to the impossibility of producing sulfur-containing amino acids such as methionine or cysteine, and phosphate restriction stops the biosynthesis of nucleic acids. In these two cases, there is an accumulation of NADPH and acetyl-CoA. This increase in energy causes the inhibition of TCA circle enzymes. Consequently, acetyl-CoA accumulates and enters the PHA circle by converting acetyl-CoA to acetoacetyl-CoA via β -ketothiolase, which can be observed in Figure 2. If the synthesis of cellular components (e.g., proteins) is blocked due to a lack of substrate, PHA synthesis starts.

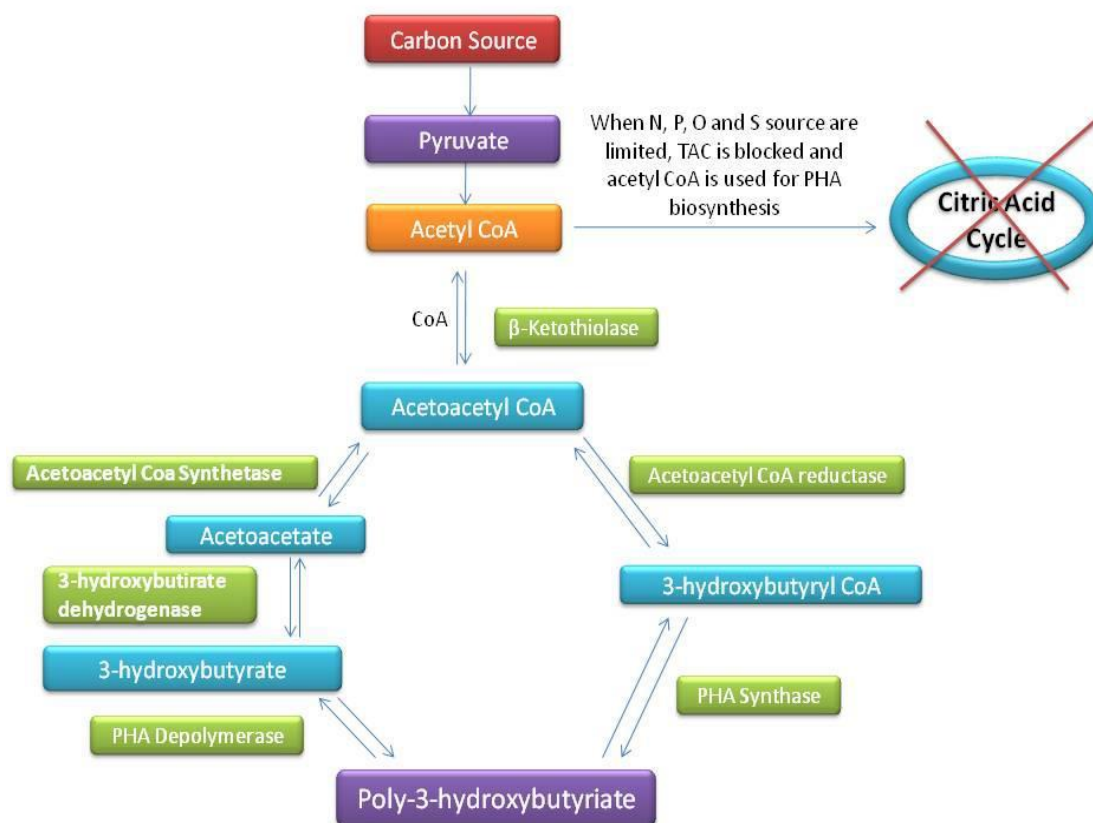


Fig. 2. Scheme of metabolic pathway I for the biosynthesis of PHB

The common biosynthetic pathway of polyhydroxybutyrate includes three different enzymes that catalyze three different reactions. Three enzymes are encoded by three different genes. In the first reaction, two molecules of acetyl coenzyme A (acetyl-CoA) condense to form acetoacetyl-CoA. This reaction is catalyzed by the enzyme β -ketothiolase encoded by the PHB gene and catalyzes the formation of a carbon-carbon bond. In the second reaction, acetoacetyl-CoA is reduced to (R)-3-hydroxybutyryl-CoA using the enzyme acetoacetyl-CoA reductase, which depends on NADPH. Acetoacetyl CoA reductase encoded by the PHBB gene. In the third reaction, PHB synthase encoded by the PHB gene catalyzes the polymerization of R-3-hydroxybutyryl-CoA in PHB. Genes encoding the enzymes responsible for the biosynthesis of PHB are located in the PHB CAB operon. The reactions are shown in Fig. 3 and 4.

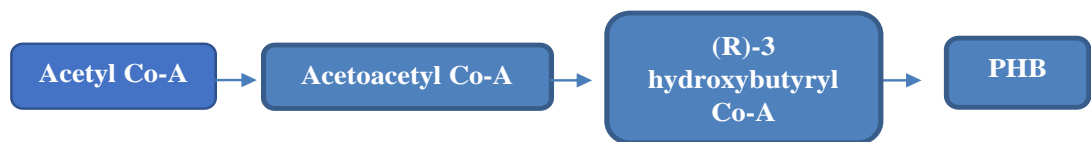


Fig. 3 Biosynthetic pathway of PHB

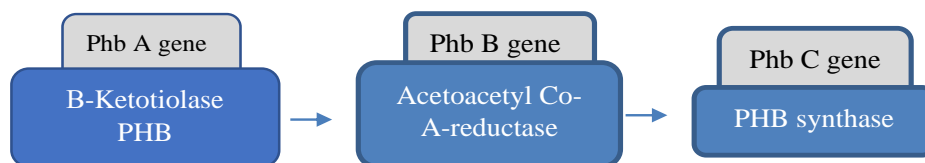


Fig.4 Genes coding enzymes responsible for biosynthesis of PHB [17, 18].

The key molecule that provides the 3-hydroxyalkanoyl-CoA substrate for the synthesis of PHA is acetyl-CoA. The substrate 3-hydroxyalkanoyl-CoA can also be obtained by β -oxidation of fatty acids. Acyl-CoA, formed on the pathway of β oxidation, passes into the process of synthesis of PHA. The precursor for the synthesis of PHA 3-hydroxyacyl-CoA is supplied in the process under the action of various enzymes. Such enzymes are 3-ketoacyl CoA reductase, epimerase, (R) enoyl CoA hydratase / enoyl CoA hydratase 1, acyl CoA oxidase, and enoyl CoA hydratase 1 [18].

Glucose metabolism. PHA is produced from a wide range of substrates, such as renewable resources (sucrose, starch, cellulose, triacylglycerols), fossil resources (methane, mineral oil, lignite, coal), by-products (molasses, whey, glycerin), chemicals (propionic acid, 4-hydroxybutyric acid) and CO₂. The bulk of PHA is produced by microorganisms that catabolize glucose along the Enter-Doudoroff (KDPG) pathway, which is found only among prokaryotic organisms [19]. The end product of this pathway is pyruvate, which can be converted by the pyruvate dehydrogenase enzyme system into acetyl-CoA, a key compound in the direction of the TCA circle and PHA biosynthesis, as shown in Figure 5.

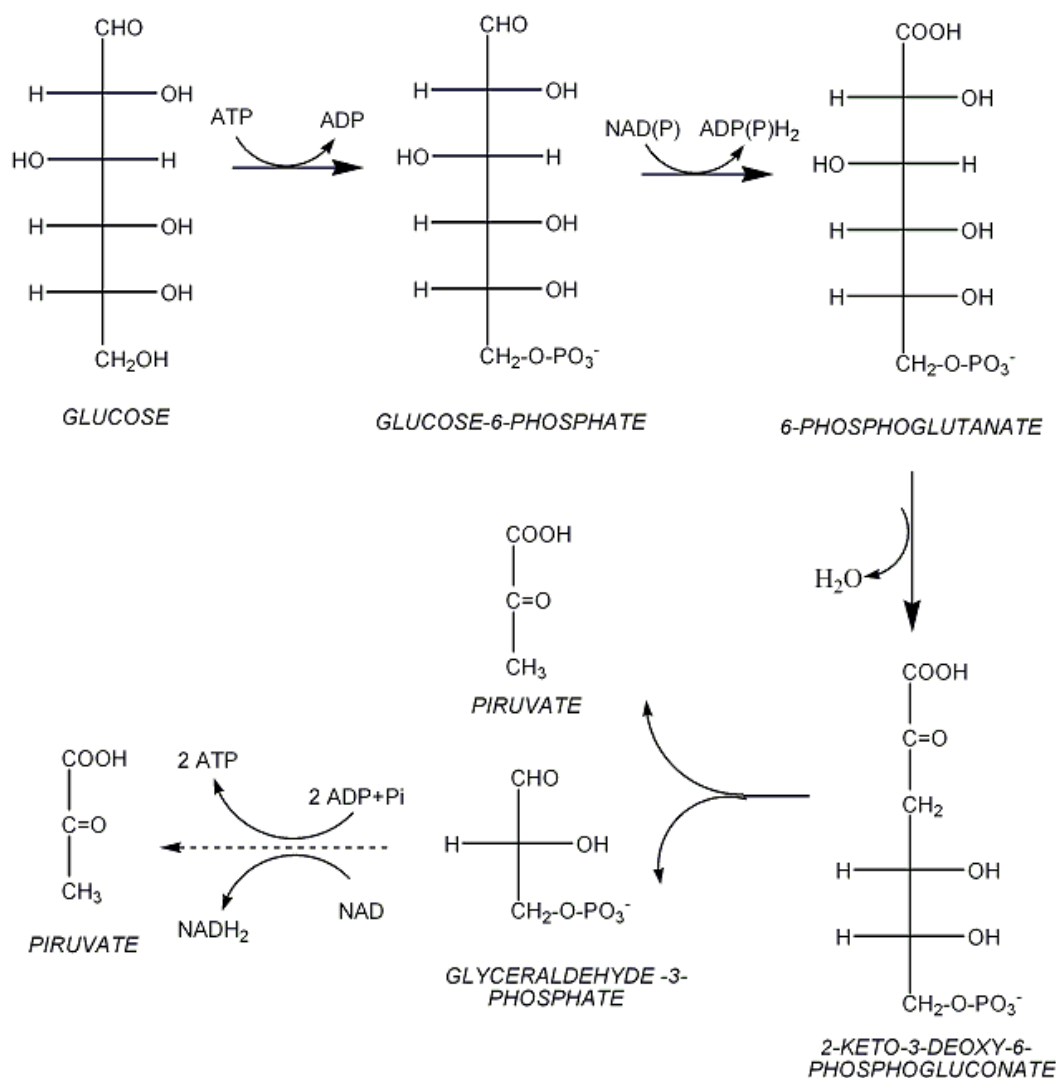


Fig. 5. Glucose metabolism via the Entner-Dudorov path.

Methods for improving the synthesis of PHB. The drawback of the widespread use of PHA is the fact that in most cases their production costs are higher than the costs of conventional petroleum-based plastics. To overcome this problem and be competitive face-to-face with traditional plastics, PHA must have a large production volume at low cost. The high cost of production of PHA is mainly due to the high cost of raw materials, small volumes of production and high costs of processing, especially for the purification and isolation of the polymer.

The cost of the carbon source makes a significant contribution to the total cost of production of PHA, amounting to about 40-50% of the total cost of production. The trend is to use cheaper feedstock, which does not interfere with the needs of food or feed production, for the production of biopolymers [20-22]. Table 1 summarizes the cost of some types of raw materials already used for the production of PHA [23].

Table 1. The effect of the cost of the substrate on the cost of production of PHBs

No.	Substrate	Estimated price (€ / kg)	The output of PHB (g PHB / g substrate)
1.	Glucose	0.41	0.38
2.	Sucrose	0.35	0.40
3.	Ethanol	0.31	0.50
4.	Methanol	0.28	0.43
5.	Acetate	0.59	0.38
6.	Cassava starch	0.19	0.20
7.	Cheese whey	0.07	0.33

8.	Reed treacle	0.10	0.42
9.	Palm oil	0.79	0.65
10.	Soybean oil	0.92	0.70

The main goal remains the correlation of the economic effect with the use of cheaper raw materials, with obtaining a producer with high polymer synthesis.

The synthesis of PHA can be carried out by chemical or biological method. High molecular weight PHAs can be obtained when they are synthesized by biological approaches. But the structure of PHAs cannot be predicted when they are biologically obtained [24].

Débora Jung Luvizetto Facci [25] evaluated the effect of oxygen transfer rate on intracellular P (3HB) accumulation in order to increase P (3HB) synthesized by *Bacillus megaterium* DSM 32 T in batch bioreactor cultures. Cultivation on a bioreactor on a laboratory scale was carried out at various volumetric oxygen mass transfer coefficients, $k_L a$, when the stirring speed was set to preset values. The results of this work show that oxygen transfer is a key factor in the accumulation of P (3HB) *B. megaterium*, increasing the intracellular mass fraction of P (3HB) from 39% to 62% CDW for $k_L a$ condition 0.006 eva^{-1} .

Scientists from the Institute of Biochemistry. A.N. Baha Kosmachevskaya O.V. [26] and others in their study studied the synthesis of poly-3-hydroxybutyric acid (PHB) in the cells of nodule bacteria *Rhizobium phaseoli* grown in deep culture. We modified the Low method for determining PHB, which allowed us to isolate and determine the amount of polymer directly in biomass. Only S-forms of *R. Phaseoli* cells were capable of synthesizing PHB. On a carbon-rich medium, the accumulation of PHB was stronger (by about 50%), and the polymer granules were more pronounced. The synthesis of PHB increased with decreasing aeration, and the maximum content was reached by 35–40 h of growth. The effect of oxidative stress caused by tert-butyl peroxide and benzyl viologen on the growth of bacteria synthesizing PHB was studied. Both substances negatively affected the growth of bacteria, while growth was restored only in the S-form synthesizing PHB. It can be concluded that PHB is a protector for nodule bacteria under oxidative stress. The maximum content of PHB in *R. Phaseoli* cells reached 54% of the dry cell mass. This value is close to the values characteristic of bacterial strains - polymer producers used in biotechnology. It can be concluded that nodule bacteria grown in deep culture may be potential producers of PHB and other polyhydroxyalkanoates.

Methods to optimize the composition of the nutrient medium and certain conditions for improving the production of PHB are insufficient, therefore, scientists Grage K. et al. [27] have developed bioengineering to form functional inclusions of PHB in the gram-positive bacterium *Bacillus megaterium*, which is free of LPS and is well established in industrial production. Since *B. megaterium* is a natural producer of PHB, a PHB-negative strain PHA 05 was used to avoid any background production of PHB. Plasmid-mediated T7 promoter expression of genes encoding β -ketothiolase (Pha A), acetoacetyl-CoA reductase (Pha B) and PHB synthase (Pha C) allowed the production of PHB in *B. megaterium* PHA05. To obtain functionalized inclusions of PHB, the N- and C-terminus of PHAC were fused with four and two IgG-binding Z domains from *Staphylococcus aureus*, respectively. The PHA ZZ domain fusion protein was strongly produced on the surface of PHB inclusions, and it was found that the corresponding isolated ZZ domain containing PHB granules purifies IgG with a binding capacity of 40-50 mg IgG / g granules. As *B. megaterium* has the ability to form spores and the corresponding endospores could interact with cellular Purify inclusions, the negative sporulation production strain was generated by disrupting the spo IIE gene in PHA05. This strain did not produce spores when

tested under conditions causing sporulation, and it was still able to synthesize PHB granules with the ZZ domain.

Data of scientists Noha S. Elsayed et.al. [28] described in the article on the production of poly (3 - hydroxybutyrate) isolate *Azomonas macrocytogenes* KC685000 obtained after 24 hours of incubation of the isolate in a 14 L fermenter obtained 22% poly (3-hydroxybutyrate) (PHB) dry biopolymer cell mass (CDW) using aeration of 1 μm , 10% inoculum size and an initial pH of 7.2. To control the fermentation process, the Logistic and Leudeking - Piret models were used to describe cell growth and PHB, production, respectively. These two models are in good agreement with experimental data confirming the growth, the associated nature of the production of PHB. The best of method for recovering PHB was chemical digestion using sodium hypochlorite alone. The obtained polymer was characterized using FT-IR, ^1H NMR spectroscopy, gel permeation chromatography, and a transmission electron microscope. Analysis of the nucleotide sequences of the PHA synthase enzyme revealed the tertiary structure of the PHA synthase enzyme, it was analyzed using the modular software approach for predicting structural classes, the Tied Mixture Hidden Markov Model server and the Swiss model software. It was found that the structural class of PHA synthases was a multi-domain protein (α / β) containing a conserved cysteine residue and lipase block as characteristic features of the α / β hydrolase superfamily. Taken together, all molecular characterization results and images obtained using a transmission electron microscope confirm that the formation of PHB was achieved by improving the model. To our knowledge, this is the first report on the production of growth-related PHB using *A. macrocytogenes* isolate. KC685000 and its PHA-synthase class III.

A study by Mohamed M. Khattab and Yaser Dahman [29] describes the production and recovery of poly (3 hydroxybutyrate) P (3HB) from agricultural waste. The production was carried out using the *Ralstonia eutropha* strain with sugars of hemp biomass hydrolysates Hard as a carbon source and ammonium chloride as a nitrogen source. The results show that a maximum hydrolysis yield of 72.4% was achieved with a total sugar hydrolysate concentration (i.e. glucose and xylose) of 53.0 g / L. The sugar metabolism in *Ralstonia eutropha* has shown preference for glucose metabolism over xylose. Under optimal conditions, cells can accumulate P (3HB) polymer in an amount of up to 56.3 wt. % dry cells. This corresponds to a total production of 13.4 g / l (productivity 0.167 g / l h). The nitrogen source did not show a negative effect on P (3HB) biosynthesis, but rather on cell growth. Among several methods investigated, using the ultrasonic assistant sodium dodecyl sulfate (SDS), extracted bioplastics directly from the broth cell concentrate with a P (3HB) content of 92%. The number average molecular weights (M_n) of the final reduced bioplastics were in the range of 150–270 kDa with the polydispersity index (M_w / M_n) in the range of 2.1–2.4.

A study by Songsri Kulpreecha et al. [30] Aimed at increasing cell density and producing homopolymer polyhydroxybutyrate (PHB) by *Bacillus megaterium* BA-019, using renewable and inexpensive bioresources as a substrate. A higher cell density and a higher level of PHB production was obtained using sugarcane and urea molasses as sources of carbon and nitrogen, respectively, nitrogen restriction at a molar ratio of C / N 25 led to increased cell growth and PHB production in batch cultures. Fed batch cultivation with a nutrient consisting of MSM with sugarcane molasses, urea and trace elements, and controlled by controlling the pH-stat, leads to a significant increase in cell concentration and PHB production. Optimal for supplying a nutrient medium in this system, a higher total sugar concentration (400 g / l) and a C / N molar ratio of 10 mol / mol are required. Under these conditions, the highest achieved cell mass (72.6 g / L DW) and the PHB content (42% of the dry cell

weight) were achieved in a short time, the cultivation time (24 hours), which leads to an increase in the productivity of PHB (1.27 g / l / hour). However, dissolved oxygen was limiting and, therefore, the system is likely to be suboptimal and capable of even further improving the rate of PHB production.

To add value to biomass, waste from agriculture, food processing plants and municipal organic waste can be used to produce biopolymers such as biohydrogen and biogas through various microbial processes. In fact, various bacterial strains can synthesize biopolymers to convert waste into valuable intracellular (e.g. polyhydroxyalkanoates) and extracellular (e.g. exo polysaccharides) bio products that are useful for biochemical production. In particular, a large number of bacteria, including *Alcaligenes eutrophus*, *Alcaligenes latus*, *Azotobacter vinelandii*, *Azotobacter chroococcum*, *Azotobacter beijerincki*, *methylophilus*, *Pseudomonas* spp., *Bacillus* spp., *Rhizobium* spp., *Escherichia*., used for the production of polyhydroxyalkanoates on an industrial scale from various types of organic by-products. Thus, the development of highly effective microbial strains and the use of by-products and waste as substrates can reasonably make the costs of producing biodegradable polymers comparable to those needed for plastics derived from petrochemicals and stimulate their use. Many studies report the use of the same organic substrates as alternative energy sources for the production of biogas and biohydrogen by anaerobic digestion, as well as the processes of darkness and photo fermentation under anaerobic conditions. Therefore, the simultaneous production of bioenergy and biopolymers at a reasonable price through an integrated system becomes possible using by-products and waste as sources of organic carbon. Overview of suitable substrates and microbial strains used in inexpensive polyhydroxyalkanoates for the production of biohydrogen and biogas. The possibility of creating a unique integrated system is being discussed, as it represents a new approach for the simultaneous production of energy and biopolymers for the plastic industry using by-products and waste as sources of organic carbon [31].

Azotobacter vinelandii OP is a bacterium that produces poly (3-hydroxybutyrate) (PHB). Díaz-Barrera et al. [32] evaluated the production of PHB in a stirred bioreactor using various oxygen transfer strategies. Using different oxygen content in the inlet gas, the oxygen transfer rate (OTR) was changed at a constant mixing speed. Periodic cultures were carried out without monitoring the dissolved oxygen tension (DOT) (using 9% and 21% oxygen in the inlet gas) and under the control of DOT (4%) using gas mixing, the culture was grown on a medium with sucrose. Cultures that developed without DOT control were limited to oxygen. As a result of changes in the oxygen content in the inlet gas, OTR decreases (4.6 mmol l⁻¹ h⁻¹) and the specific oxygen absorption rate (11.6 mmol g⁻¹ h⁻¹) was obtained using 9% oxygen in the inlet gas. The use of 9% oxygen in the inlet gas was most suitable for improving the content of intracellular PHB (56 ± 6 wt. %). For the first time, PHB accumulation in *A. vinelandii* OP culture developed with different OTRs was compared under conditions of homogeneous mixing, demonstrating that bacterial respiration affects the synthesis of PHB. These results can be used to develop new oxygen transfer strategies for the production of PHB under production conditions.

Kulpreecha et al. [33] tested *B. megaterium* BA-019 on sugarcane molasses (20 g / l) as a carbon source and urea or ammonium sulfate at 0.8 g / l as the studied nitrogen sources. In these experiments, a cell dry matter concentration of 72.7 g / L was achieved in 24 hours with a PHB content of 42%. In conditions of limitation of nitrogen operating in recharge mode. In addition, with sugarcane, *C. necator* showed the best concentration of PHA among bacterial strains (recombinant *E. coli*, *A. vinelandii* UWD, and *B. megaterium*) working in the mode of feeding with molasses

as a carbon source. In fact, *C. necator* is able to accumulate approximately 100 g / l of synthesizing glucose (from starch) and sucrose (from sugarcane).

Ramdane Haddouche et al. [34] found the ability to produce polyhydroxyalkanoates (PHA) by recombinant strains of oil-containing yeast *Yarrowia lipolytica* expressing the PHA synthase gene (PHAC) from *Pseudomonas aeruginosa* in peroxisome. The yield of PHA, but not the composition of the monomer, depended on the POX genotype (coding for POX acyl CoA oxidase genes). In this study of variants of *Y. lipolytica* β -oxidation is a multifunctional enzyme, with deletions or inactivation of the R-3-hydroxyacyl-CoA-dehydrogenase domain, we were able to obtain heteropolymers (functional enzyme MFE) or homopolymers (without 3-hydroxyacyl-CoA-dehydrogenase activity) PHA consisting mainly of 3-hydroxyacid monomers (> 80%) of the same length as the external fatty acid, used for growth redirection of the flow of fatty acids towards β -oxidation deletion of the neutral lipid synthesis pathway (mutant strain Q4 lacks acyl transferase encoded by LRO1, genes DGA1, DGA2 and ARE1) combined with one expressing only domain enoyl-CoA hydratase 2, resulted in a significant increase in the level of PHA, up to 7.3% of sub. mass cells. Finally, the presence of shorter monomers (up to 20% of monomers) in the mutant strain lacking the peroxisomal 3-hydroxyacyl-CoA dehydrogenase domain provided evidence for partial mitochondrial β -oxidation in *Y. Lipolytica*.

In a study by Tripathi A.D. et al. [35], Depending on availability and cheaper costs, various carbon sources were tested for the production of PHA (polyhydroxyalkanoates) by the soil bacterium *Pseudomonas aeruginosa*, and it was found that the waste from the sugar factory (cane molasses) yields a maximum PHA (biodegradable polymer). Urea served as a powerful source of nitrogen compared to other inorganic sources of nitrogen in the synthesis of bioplastics. The influence of various physical parameters, namely; pH, temperature and mixing speed were also studied at the PHA. The kinetics of periodic cultivation under optimized cultural and physical conditions showed a maximum cell mass and PHA concentration of 7.32 ± 0.2 and 5.60 ± 0.3 g / l, respectively, after 54 hours of cultivation. Sugar factory waste (total sugar 4%) and urea (0.8%) improved the efficiency of the process, which showed a yield (Y P / X) of 0.70 at a rate of 0.11 g / l / h. PHA was further characterized as PHB using infrared spectroscopy with Fourier transform (FT-IR).

Scientists Myshkina V.L. from the Institute of Biochemistry. A.N. Bakha [36] RAS the ability of the *Azotobacter chroococcum* 7B strain, producer of polyhydroxybutyrate (PHB), to synthesize its copolymer poly-3-hydroxybutyrate-3-hydroxyvalerate (PHB - GV) was studied. It was shown for the first time that the *A. chroococcum* 7B strain is able to synthesize PHB-HB with a different molar percentage of the inclusion of hydroxyvalerate (HB) in the polymer chain when grown on sucrose medium with the addition of carboxylic acids as precursors of the HB units in the PHB chain: valerianic (from 13.1 to 21.6 mol%), propionic (3.1 mol%) and hexanoic (2.1 mol%) acids. The qualitative and functional difference between PHB and PHB-HB is shown by the example of the kinetics of the yield of methyl red from films made from synthesized polymers. The maximum inclusion of HS in the polymer chain (28.8 mol%) was noted with the additional introduction of 0.1% peptone into the nutrient medium against 20 mM valerate. The data obtained allow us to consider the strain as a potential producer of not only PHB, but also PHB-HB.

According to the methods of cultivation of PHB synthesizing bacteria, A. Nemoykina [37] in her work, she estimated the accumulation of alginate and PHB synthesizing *Azotobacter vinelandii* BIMB216 bacteria when cultured in flasks with different mixing frequencies. At a stirring frequency of 200 rpm, a high conversion

of the carbon source to alginate was observed, while at 100 rpm the carbon source was converted to PHB. The maximum biomass concentration was obtained in cultures grown at 200 rpm 4.2 ± 0.1 g / l.

Analysis of the literature indicates the active development of research aimed at studying the synthesis and structure of polymers based on derivatives of carboxylic acids, table 2 presents a list of PHA-producing bacteria and used renewable sources.

Table 2. List of PHA-producing bacteria and renewable sources used

Substrate used	Strain	PHA (g/L)	PHA (%)	References
Pea flour	<i>Rhizobium phaseoli</i>		54	[27]
Lb	<i>Azomonas macrocytogenes</i> KC685000	0,3	22	[29]
Lignocellulosic substrate	<i>Ralstonia eutropha</i>	1,3	56,33	[30]
Sugarcane and urea stocks as carbon sources	<i>Bacillus megaterium</i> BA-019	1,27	42	[31]
Sucrose and Oxygen Medium	<i>Azotobacter vinelandii</i>	56 ± 6		[33]
Sugarcane	<i>C. necator</i>	1,2	42	[34]
Tridecanoic acid	<i>Yarrowia lipolytica</i>		7,3	[35]
Sugar factory waste (cane molasses)	<i>Pseudomonas aeruginosa</i>	$5,60 \pm 0,3$		[36]
Carbohydrate medium with different mixing frequencies	<i>Azotobacter vinelandii</i> BHM B216	4,2		[38]
Cashew apple, Jawar stem, Neera	<i>Bacillus subtilis</i>	0.027, 0.034, 0.284		[39]
Cashew Apple, Jawar Stem, Neera	<i>Bacillus cereus</i>	0.054, 0.049, 0.152		[39]
Sugarcane Bagasse, Grapes Pulp,	<i>Bacillus megaterium</i>	0.198, 0.006, 0.079		[39]
Beet molasses	<i>Bacillus megaterium</i> , <i>Bacillus Cereus</i> , <i>Bacillus subtilis</i>		41, 25, 0.5	[40]
Card board industrial effluent	<i>Bacillus sp.</i> NA10	3.952		[41]
Volatile fatty acids	<i>Ps. putida</i> CA-3	1.56	39	[41]
Fatty acids	<i>Ps. putida</i> Bet001	9.8-15.5	49.7-68.9	[42]

Methods for determining PHB. Careful screening of producer bacteria is the basis of the experiment, and today there are two main methods for detecting PHB of synthesizing bacteria from the environment, namely, screening based on the phenotype and based on the genotype. There are many phenotypic discoveries of methods for detecting intracellular granules of PHA that are used to screen manufacturers of PHA, including staining Sudan with black B [43]. Nile blue A staining [44] and Nile red, resulting in dark blue or fluorescent granules. Alternative staining methods have been developed to directly stain colonies or grow bacteria on plates containing Nile Blue A or Nile Red, resulting in fluorescent colonies that can be visualized using UV light. Colonies producing PHA on dishes containing black Sudan B appear black and blue [45]. It was reported that PHA stained with Nile red exhibit similar fluorescence behavior, with a maximum at a radiation wavelength between 540 and 560 nm and a radiation wavelength between 570 and 605 nm, detected by fluorescence spectroscopy or flow cytometry. This is suitable for

analyzing the size distribution of granules in biotechnology. Staining of cell suspensions during cultivation experiments showed that Nile red has a high potential for the quantification of hydrophobic bacterial polyhydroxyalkanoic acids. Such optical methods offer the advantages of real-time online monitoring with high specificity.

In the work of O. V. Kosmachevskaya [26], a solution of Nile red in dimethyl sulfoxide, 0.55 mg / ml, was used. Cells selected at a certain stage of growth were destroyed by ultrasound. The destroyed cells were centrifuged and resuspended in water to $A_{600} = 0.1$. To 3 ml of a suspension of destroyed cells was added 41 μ l of a solution of Nile red to a final concentration of 7.5 μ g / ml. The suspension was incubated for 30 min in the dark at room temperature. Stained samples were centrifuged and resuspended in 3 ml of water. Studies have also been conducted with whole cells. In this case, a Nile red solution was added to 3 ml of a standardized cell suspension. A further procedure was performed as described above. Stained cells were centrifuged and resuspended in 3 ml of water.

The content of PHB in biomass in the work of V. A. Ezhov et al. [46] From methanol *Methylobacterium halotolerans* C2 was determined by reverse phase HPLC on a SIX C18 column (5 μ m). For this, samples of dry biomass hydrolyzed conc. H₂SO₄ at 100 ° C for 1 h, then the hydrolyzate was neutralized with 5 N NaOH and centrifuged for 20 min at 5000 g. The supernatant was applied to the column and eluted with methanol – water (1: 1) at a rate of 0.4 ml / min. The PHB content in the eluates was determined spectrophotometrically at 228 nm using a UVIS 200 UV detector (Linear, United States) using a calibration curve.

Batch fermentation was carried out in 250 ml Erlenmeyer flasks containing 100 ml of culture medium. The flasks were inoculated and kept at 30 ° C and 130 rpm for the required time. For large-scale production, a 10-liter bioreactor was used that contained 4 L of culture medium.

Cells were harvested by centrifugation at 10,000 rpm. for 10 min in a centrifuge (Heraeus Sepatech Biofuge 28 Rs, Germany) at 20 ° C and lyophilized in the laboratory.

The polyhydroxybutyrate polymer obtained by the selected PHB-positive isolates is isolated and quantified using the sodium hypochlorite method given by Lawand Slepecky with slight modifications [47-48]. The amount of PHB produced is calculated with reference to a standard curve prepared using pure PHB (Sigma-Aldrich) [49].

DISCUSSION and CONCLUSIONS

The development of PHA in the mass chemical industry will solve at least three problems: the use of petroleum for plastic materials, the reduction of CO₂ emissions and environmental protection. This is due to the sustainable development of the chemical industry. To reduce the cost of producing PHA, much more work needs to be done so that PHA-based biofuels can be added to existing bio-based fuels, including ethanol, propanol, butanol, biodiesel, hydrogen and methane gas.

Based on a literature review, physical parameters are established that are a key factor for the accumulation of PHB, namely: pH, temperature, mixing speed and oxygen transfer. The kinetics of batch cultivation under optimized cultural and physical conditions showed maximum cell mass and PHA concentration. The synthesis of PHB increased with decreasing aeration, and the maximum content was reached up to 66%.

The protective function of PHB for bacteria is to mobilize energy reserves in case of stressful situations, including a lack of carbohydrates. It is known that PHB

can protect the cell from other stressful effects: heat and osmotic shock, UV radiation, the effects of oxidizing agents. PHB accumulates in prokaryotic cells under conditions of unbalanced growth and acts as a reserve substance for storing carbon and energy, like fat, glycogen and starch in animals and plants. These biopolymers have a number of specific properties, such as biodegradability and compatibility with living body tissue, which opens up great opportunities for their use in practice. The final product of the biodegradation of PHB in the environment is water and carbon dioxide, and in a living organism 3-butobutyric acid.

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ҚАЙТА ЖАҢАРТЫЛАТЫН КӨЗДЕРДЕН АЛЫНАТЫН ПОЛИГИДРОКСИБУТИРАТТАРДЫ МИКРОБИОЛОГИЯЛЫҚ ӨНДІРУ

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ТҮЙІН

Пластмассалар күнделікті өмірімізде маңызды рөл атқарады және әртүрлі мақсаттарда қолданылады. Экологиялық таза өнімдердің өндірісі бүгінде биопластиканы қосқанда белсенді дамып келеді. Қазіргі уақытта ғалымдар әртүрлі микроорганизмдер қосалқы зат ретінде синтезделетін полигидроксibuтираттар сияқты полигидроксиланоканаттар немесе оның қосалқы типтері сияқты сонымен қатар кәдімгі синтетикалық пластмассалардың орнына қолдануға болатын биологиялық ыдырайтын полимерлерге үлкен назар аударады. Алайда, мұндай биологиялық ыдырайтын полимердің ірі көлемдегі өндіріс құны оның кең таралуына бәсекеге қабілетті емес. Полигидроксibuтираттар микроб өндірісін зерттеу экономикалық тұрғыдан тиімді субстраттарды анықтауға, сонымен қатар өндіріс үшін дененің тиісті штамдарын анықтауға бағытталуы керек. Бұл биополимерлер бірқатар биологиялық ыдырау және тірі дене ұлпаларымен үйлесімділік сияқты бірқатар ерекше қасиеттерге ие, бұл оларды практикада қолдануға үлкен мүмкіндіктер береді. Қоршаған ортадағы полигидроксibuтираттар биodeградациясының соңғы өнімі су мен көміртегі диоксиді, ал тірі организмде 3-изомеразды қышқылы. Бұл шолудың негізгі бағыты бактериялардың әртүрлі түрлерін қолдана отырып, әртүрлі экономикалық субстраттардан биопластик өндіруге бағытталған.

Негізгі сөздер: биополимер, полигидроксибутират, полигидроксиалканонат, қалпына келтірілетін қайнар көз, микроб өндірісі, арзан көміртек көздері; мерзімді өсіру.

МИКРОБИОЛОГИЧЕСКОЕ ПРОИЗВОДСТВО ПОЛИГИДРОКСБУТИРАТОВ ИЗ ВОЗОБНОВЛЯЕМЫХ ИСТОЧНИКОВ

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АБСТРАКТ

Пластмассы играют важную роль в нашей повседневной жизни и используются для различных целей. Индустрия экологических продуктов в наше время активно развивается, в том числе биопластиков. Большое внимание ученых привлекают биоразлагаемые полимеры типа полигидроксиалканонаты или полигидроксибутираты, которые синтезируются различными микроорганизмами как запасное вещество и, к тому же, являются наиболее приемлемой заменой обычных синтетических пластиков. Однако стоимость крупномасштабного производства такого биоразлагаемого полимера не является конкурентноспособной его широкому распространению. Исследования микробной продукции полигидроксибутиратов должны быть направлены на выявление экономически эффективных субстратов, а также определение подходящего штамма организма для производства. Эти биополимеры обладают рядом специфических свойств. Например, способность к биодеструкции и совместимость с живой тканью организма, что открывает большие возможности для их использования в практике. Конечным продуктом биodeградации полигидроксибутиратов в окружающей среде является вода и двуокись углерода, а в живом организме – 3-изомасляная кислота. Основное внимание в этом обзоре уделено производству биопластиков из различных экономичных субстратов с использованием различных видов бактерий.

Ключевые слова: биополимер, полигидроксибутират, полигидроксиалканонат, возобновляемый источник, микробное производство, дешевые источники углерода, периодическая культура.